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## Catalytic Production of Syngas by Methane Reforming

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The research on methane reforming has recently gained considerable attention and proved the scientific interest as a way of producing hydrogen through the generation of synthesis gas (mixed gas of hydrogen and carbon monoxide). The conversion of syngas can be conducted by steam reforming and dry reforming, using  $H_2O/CH_4$  or  $CO_2/CH_4$  as feed gas respectively. Dry reforming of methane (DRM) process can achieve a higher  $CO/H_2$  product ratio (3:1) than that of steam reforming (1:1). Additionally, DRM has also received attention from the environmental consideration since the emission of methane and carbon dioxide into the atmosphere causes undesirable effect on global warming through the greenhouse effect, and these harmful gases can be simultaneously converted into useful syngas [1].

Ni and Co catalysts were the first studied for DRM by Fischer and Tropsch in 1928. However, these catalysts were observed to be severely deactivated due to carbon deposition [2]. Since then, the researchers dedicated to pursue the high efficient and coke-resistant catalysts for DRM and numerous materials like Ni, Co, Fe and noble metal (Pt, Rh, Pd, Ir) have been reported to be active for DRM [3-5]. Precious metals are proved to be less sensitive to coking as compared to Ni and the addition of second metals (alkali earth and rare earth metals) is of importance to reduce carbon deposition. Arandiyan et al. [6], synthesized the tri-metallic perovskite mixed oxides LaNi, Fe1, O3 for the reforming of CH, to syngas and found the substitution of Fe in Ni perovskite catalyst affect the product rate and promote the stability. They also discovered that introducing O<sub>2</sub> with the feed gas flow can accelerate the decomposition of carbon and thus prevent the catalytic deactivation. The effect of modification with alkali metals (M=Li, Na, K) in  $M_x La_{1-x} Ni_{0.3} Al_{0.7} O_{3-d}$  was investigated for DRM to produce syngas [1]. The Na incorporation in La site in the perovskite enhanced the activity efficiency while the K and Li substitution increased the reduction temperature and decreased the conversion rate of CH, at the same temperature comparing with LaNi<sub>0.3</sub>Al<sub>0.7</sub>O<sub>3-d</sub> catalyst. However, the substituted catalysts with alkaline metals showed significant stability after 15 h on stream reaction, maintain their activity and selectivity in the production of syngas. In addition, the addition of Sr and Ca of La also showed specific influence on the activity and stability for DRM [7].

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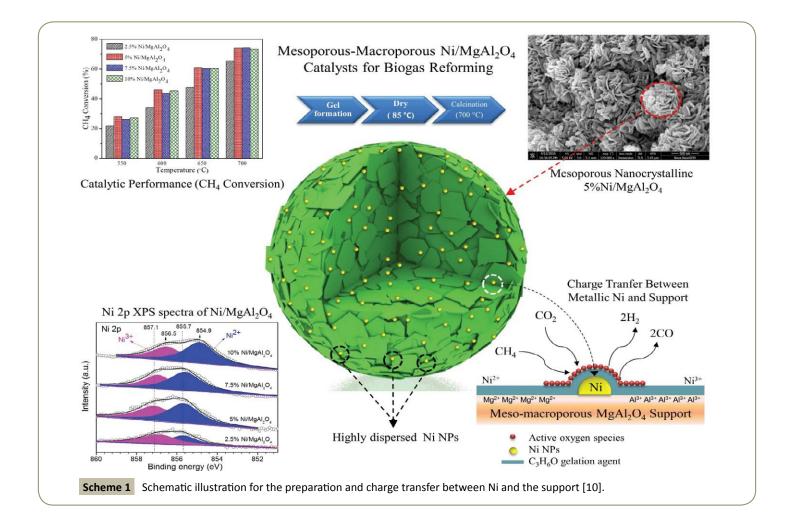
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In his recent study, Arandiyan and co-workers using a facile and simple propylene oxide assisted gelation agent route to successfully synthesize mesoporous nanocrystalline  $MgAl_2O_4$ [8,9]. The obtained spinel catalysts has large surface area in the range of 253-302 m<sup>2</sup>/g and narrow single modal pore size distributions in the mesopore region which promote the catalytic performance for  $CH_4$  reforming and resist against the carbon formation. Alternatively, they dispersed Ni nanoparticles on this mesoporous  $MgAl_2O_4$  spinel as shown in Scheme 1 and obtained an enhancement on the syngas formation from DRM [10]. The exchange of  $Mg^{2+}$  by Ni<sup>2+</sup> was observed at the low Ni loading sample (5 wt%) and this appropriate partial Ni substitution in the  $MgAl_2O_4$  spinel was believed to play a role in the elevated catalytic performance.

In the future study on DRM catalyst, the inevitable deposition of surface carbon is still a major issue. Using basic support and appropriate catalyst activation/calcination procedure, promoter to metal ratio, metal precursor is the ideal path to avoid deactivation and stable performance of the catalyst for DRM.

**2017** Vol. 2 No. 1: 5



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